

## RispEX

#### ESRA

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#### Context and objective

#### What is RispEx and what is it used for

How does it work

Validity and benchmarking



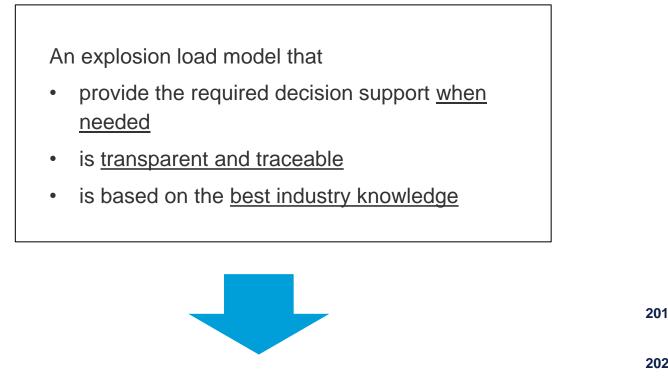


# Explosion analysis for oil and gas development projects – context

- Identified challenges:
  - Complex probabilistic explosion models with many user-influenced input parameters
  - Input with the right level of detail not available when the DeALs need to be specified
  - Still, late in detail engineering or even when asset is going into operations:
    - There is uncertainty in the input to the analysis
    - There is uncertainty in results due to complexity in model
- Experienced consequences:
  - Significant cost and weight impact on project
  - Late design changes due to significant uncertainty in DeAL
  - Significant resources spent on explosion analyses in detail engineering with limited effect on design



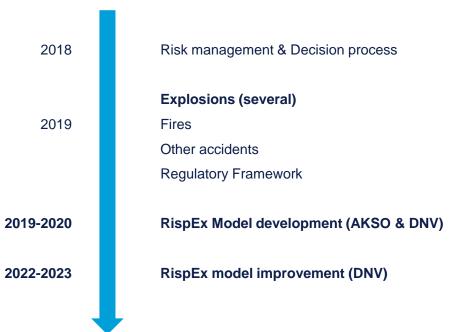
## Road to RispEx



**RispEx** 

RispEx development:

- Separate project initially performed by DNV and Aker Solutions
- Further development DNV
- Project owner has been RISP steering committee



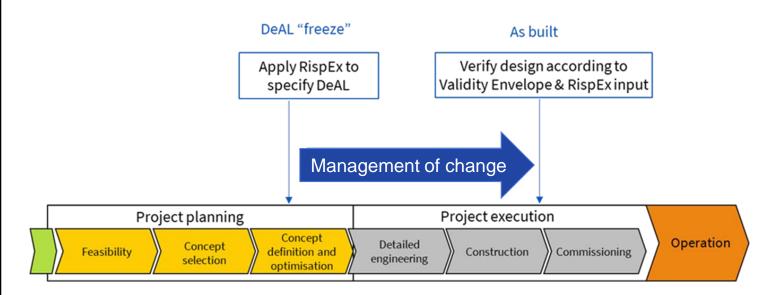
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## Overall objective RispEx tool

- The objective is to make a **digitalised** "look-up approach" based on known risk profiles
- Based on few input parameters, all known before DG2, the tool shall provide:
  - Recommended **Design Explosion Loads** for a design/module
  - Typical accidental scenarios to be used in Risk Management context (design optimization, ALARP, management of change)
- The **same safety level** shall be achieved when using RispEx vs. traditional methods
- Validity shall be clearly defined with a "validity envelope"
- Shall be available through an internet portal



### Explosion risk decision support in different phases



#### Additional needs:

- Detailing of explosion loads and other design input
- Sensitivities for ALARP and design optimisation
- Understanding the risk picture

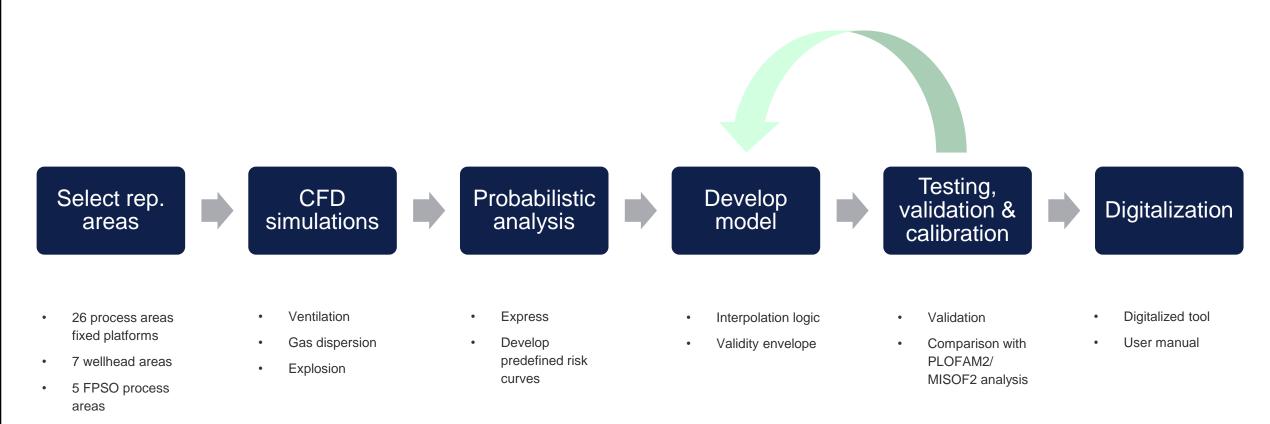
- Project planning phase:
  - Evaluate if RispEx can be used
  - Sensitivity analysis
  - Specify DeAL

#### Project Execution

- Follow-up input / basis for DeAL
- Use "Accidental scenarios" for Risk
  management purpose

Some assessments might require more detailed analysis in addition – therefore developed scenarios to be used for MoC and optimisation

#### Main steps in development

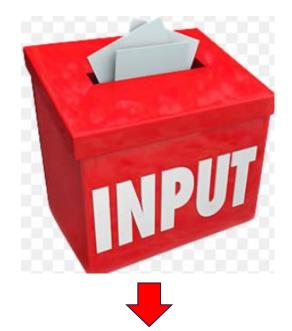


-> 38 areas in total



### Input and output of the model

- Type of concept (jacket platform, FPSO)
- Type of area (process area, wellhead area)
- Area specific input
  - Wellhead area: number of wells, Representative blowout rate category
  - Process area: Function (gas process, separation, oil process)
- Dimensions of area (provides both size and shape)
- Openness per side (provides confinement degree / explosion relief / natural ventilation conditions)
- Effect of specific strong ignition sources
- RispEx is available here: <u>RispEx</u>



#### Output

- Explosion DeAL
- Scenarios for MoC
- Frequency vs
   cloud/overpressure relations

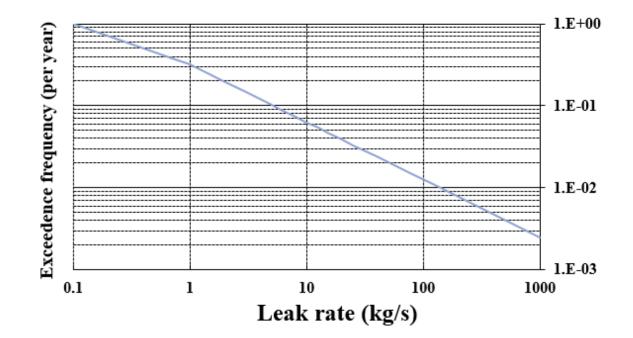
#### **Overall calculation flow**



#### Leak frequency model

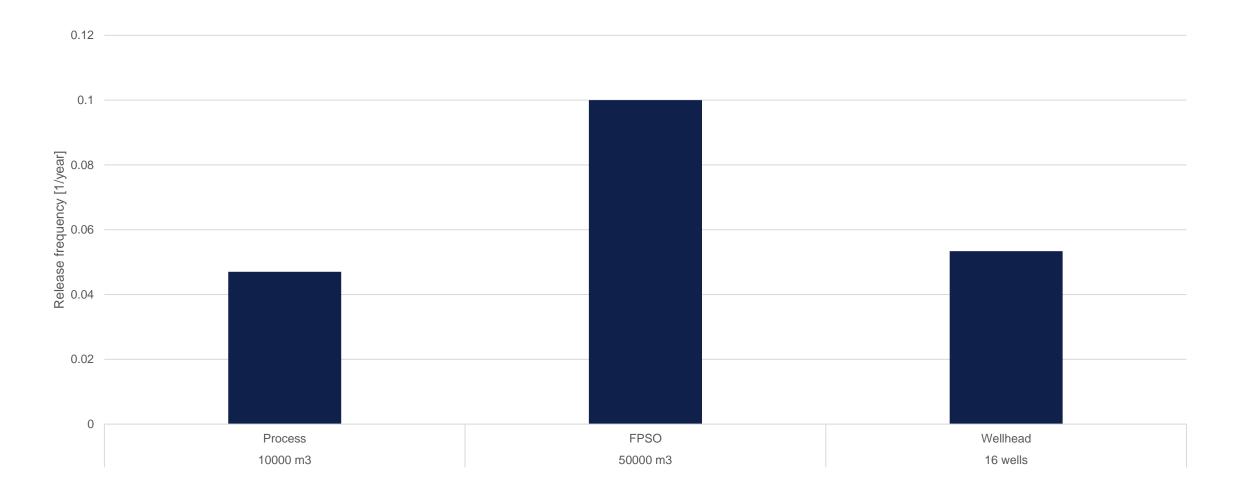


- RispEx uses a simplified leak frequency model. The total leak frequency is estimated as:
  - Proportional to the area size for process areas
  - Linearly dependent of the number of wells for wellhead areas
- For process areas the leak frequency per cube meter is applied from MISOF2 report
- For wellhead areas and FPSO process areas scaling parameters are found based on correlation with existing PLOFAM2 leak frequency analysis

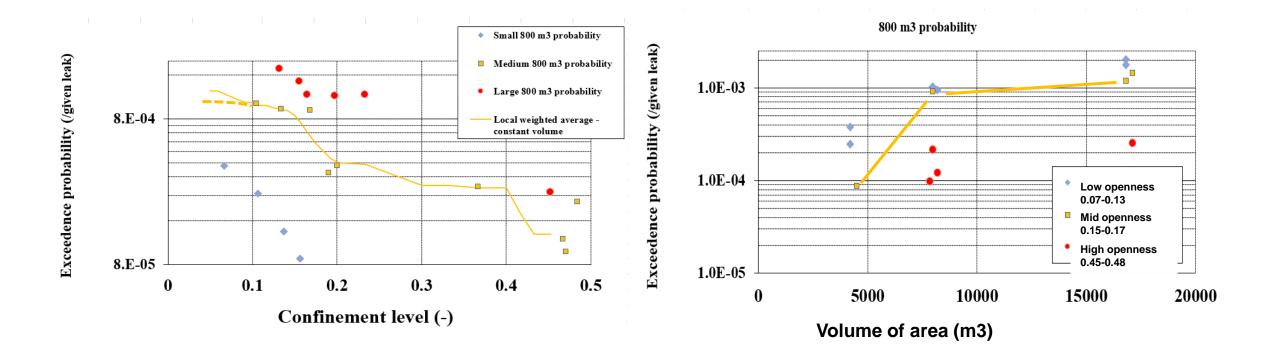


#### Leak frequency model





## Interpolation schemes Probability of exceeding 800 m3 illustrated



Cloud size vs

overpressure

relation

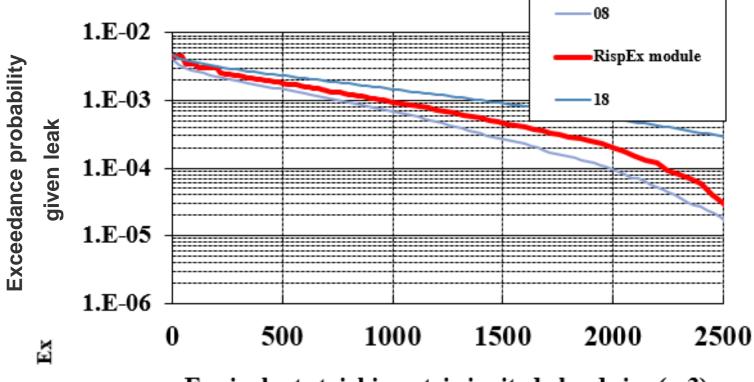
Design loads

and scenarios

## Probability vs cloud size curve



- Interpolation on volume and openness is performed to all points on the probability vs cloud size curve
- Two dimensional interpolation scheme, interpolating based on openness and volume of area



Equivalent stoichiometric ignited cloud size (m3)

#### Explosion model

- The RispEx explosion model uses a simple function to predict an overpressure caused by an ignited cloud size, with log-normal distributed term to account for the variance in the explosion pressure
- It is developed and relation between K parameter for and the area volume and area openness based on curve fitting
- Separate K values are developed for:
  - Local wall pressure
  - Local deck pressure
  - Drag



$$\frac{P_{Wall}}{P_0} = \Phi K V_f^{p_{eV}}$$

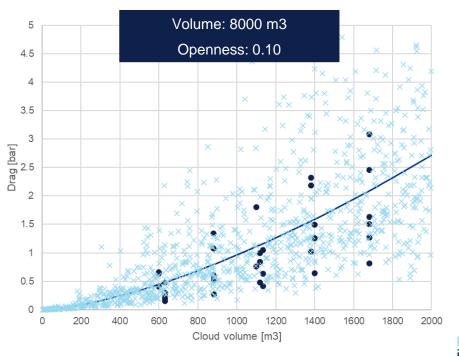
 $\frac{P_{Wall}}{P_0}$  is the calculated median pressure on the firewall.

 $\Phi$  is a lognormal stochastic variable

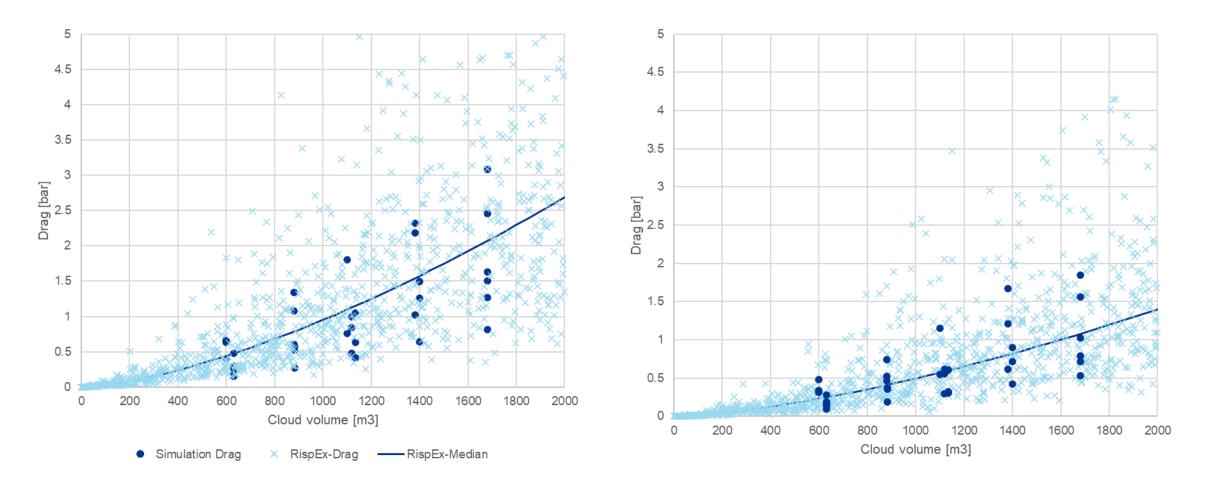
K is a fitted parameter based on volume and confinement

 $V_f$  is the volume of the stoichiometric cloud

 $p_{eV}$  is fitted a constant



#### Drag model vs Simulation results 3m (Left) and 12 m (Right)



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Cloud size vs

overpressure

relation

Design loads

and scenarios

Leak

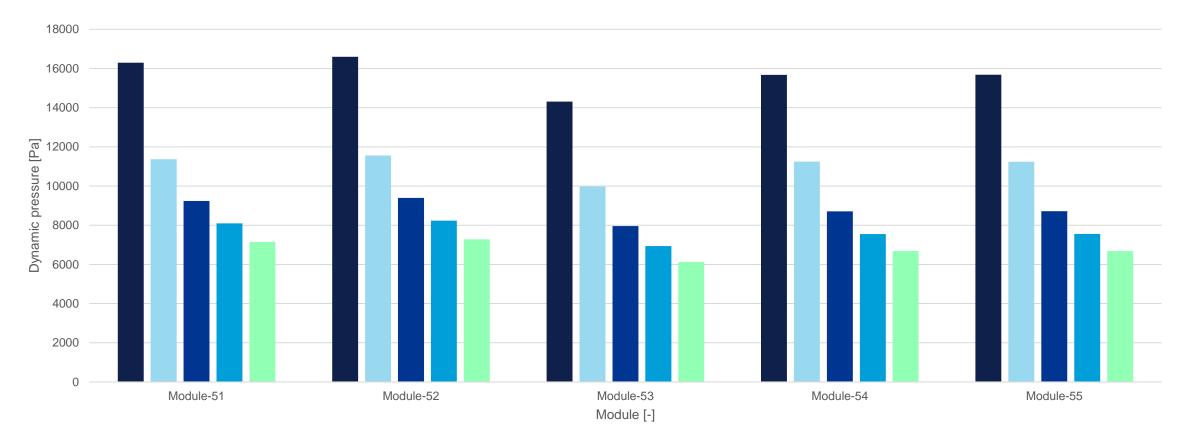
frequency

Cloud size

probabilit







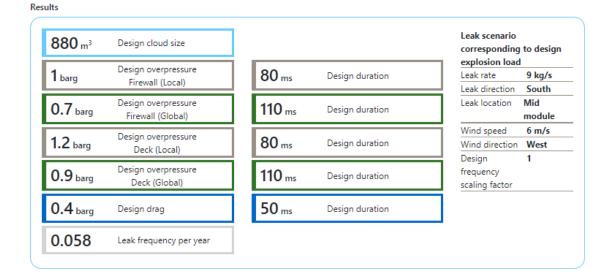
■1c ■3m ■6m ■9m ■12m



#### **Design loads and scenario**



- Design loads calculate from exceedance curves based on a default 7 x 10-5 criterion
- Criterion can be changed by changing "Design frequency scaling factor"
- Other parameters (duration and global loads) calculated based on design loads.
- Leak scenario calculated based on design cloud size and module size and confinement



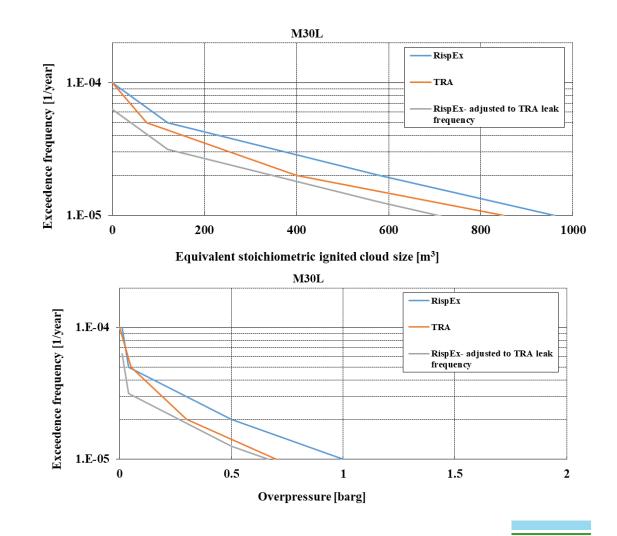
#### What can it be used for

- Within the validity envelope, RispEx shall in principle be able to replace traditional (NORSOK Z-013) explosion analysis for determining design accidental loads.
- Explosion analysis will still be required for other aspects (e.g. MOC, input to QRA and to demonstrate ALARP)

- Validity envelope consists of multiple parts:
  - Overall concept and design, e.g:
    - Design according to PSA requirements and NORSOK S-001
    - Naturally ventilated areas
    - Wind speed distribution similar to Norwegian Continental Shelf (typical)
  - RispEx user input parameters, e.g:
    - Area length, width, height.
    - Wall and deck openness
  - RispEx fixed input parameters, e.g:
    - Maximum blowdown time; 15 min to 6.9 barg
    - Max closing time ESD valves: 30 sec

### Benchmarking

- Formal benchmarking was performed as part of the initial development of RispEx.
- Further benchmarking has been performed by DNV as part of ongoing studies and the RispEx development.
- Relatively more benchmarking performed for process areas on fixed facilities compared with FPSOs.





- Many aspects of explosion risk well understood despite complex nature
- Challenges wrt to our methods from a decision support point of view
- RispEx is developed as a digitalised "look-up approach" based on the best industry knowledge
- Aim to provide explosion DeAL and other explosion risk based decision support when needed
- Simple tool with well defined input available in FEED available in an internet portal
- Output includes scenarios to be used for MoC and optimisation
- RispEx is available and can be used now



## Questions?

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